SEQUENTIAL ANAEROBIC AND AEROBIC DIRECT GAS INJECTION FOR MICROBIOLOGICAL IN-SITU REMEDIATION OF CHLORINATED HYDROCARBONS

INTRODUCTION

The overall objective of the R&D project, sponsored by AiF Germany, was the development of a new remediation approach to demonstrate which chlorinated hydrocarbons (CHC) in the groundwater can be degraded effectively in-situ using coupled anaerobic and aerobic processes. The specific innovative feature of this new approach consists of the field application of gaseous electron donors in the saturated zone. A multistage direct gas injection technology was to be developed and tested in order to enable sequential reductiveandoxidativedechlorinationofCHCcontaminated aquifers. The technology of coupled anaerobic-aerobic gas injection zones is based on mixed gas injections such as hydrogen, oxygen, argon, and in selected conditions also propane and butane. During application, targeted selective gas distributions in nonhomogeneous aquifers is to be controlled by injection pressure, injection ratio and the time length of injection intervals.

- Groundwater flow rate 1 – 10 m/d CHC concentrations 10 – 100 mg/l Depth to groundwater 2 – 3 m ▶ Aquifer base at a depth of 7 – 8 m 15 x 15 m Size of test area

- Radius of influence



downgradient plume

LABORATORY TESTS





Fig. 6: TCE degradation kinetics for various hydrogen concentrations

THE CHALLENGE

reductive dechlorination									
PCE	т	CE	cis-DCE	VC	Ethen				
CI CI CI CI				$\begin{array}{c} C = C \\ H \\ H \end{array} = C = C \\ H \\ H \\ C = C \\ C \\ H \\ C = C \\ C \\ H \\ C = C \\ C \\ H \\ C \\$	H = C = C H				
oxid deci	ative Norination	+ O ₂	+ O ₂	+ O ₂	+ O ₂				
de pro	gradation oducts	HCI	CO ₂		H ₂ O				

ig. 1: Scheme of sequential microbial chloroethene degradation steps (THIEM et al. 2008).



Fig. 2: Scheme of sequential direct gas injection rooms for stepwise reductive and following oxidative dechlorination of CHC

SITE DESCRIPTION

Down gradient of a former dry cleaning facility in Leipzig, Germany

5 m





Fig.3: Location of the Test area in the contaminated Fig.4: Base of Quaternary aquifer, well point locations, and soil profiles.

DEVELOPMENT STEPS

Fig. 5: PCE degradation kinetics for various hydrogen concentrations

RESULTS

- The successful anaerobic biodegradation of PCE and TCE as a result of applying hydrogen was proven.
- The laboratory tests provided the kinetic decay reaction factors for modeling and the dimensional basics for field application.
- An optimized Ar-H₂ gas mixture for anaerobic in-situdegradation of PCE and TCE was identified.
- Addition of CO, was shown to accelerate the CHC degradation.

CONSTRUCTION AND OPERATION OF REMEDIATION TEST FIELD INSTALLATIONS

- 6 gas injection lances
- In-situ 3D sensor array consisting of 5 sensor chains with optodes, pH sensors, ORP sensors (Oxidation-Reduction Potential), temperature sensors
- 3 TDR measuring pipes (time domain reflectometry)
- 5 gas monitoring wells
- 5 groundwater monitoring wells
- Gas dosing station with remote control.



Fig. 7: Construction of test area using SONIC drilling method and gas dosing station



Fig. 8: Overview of the gas injection and monitoring area

→ LHKW in µg/l	→ VC in µg/l	cis-1,2-Dichlor
50.000,00		
45.000,00		
40.000,00		
35.000,00		
30.000,00		
25.000,00		
20.000,00		
15.000,00		
10.000,00		
5.000,00	×	
		1
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Field installations using fast SONIC drilling method







Three gas injection series, including a successful SF₆ gas tracer test during the first injection, demonstrated the safe and faultless operation of the system components by remote control.

Exp.	Description	Gas Type and Amount	Duration of Injection
1	SF ₆ tracer test	SF ₆ (4%), H2 (3%), Ar (93%) Amount: 1,28 m ³	100 min
2	H ₂ injection in 3 lances	H ₂ (3%), Argon (97%) Amount: 3 x 6 m ³	1,740 min
3	Parallel injection of O_2 and H_2 in 2 lances	A1: Gas mixture H2 (3%), Ar (97%) A2: O ₂ -Gas (100%)	A1: 171 min A2: 226 min

Tab. 1: Type of Gas Gas Amount and Duration of Injections for 3 Field Phases.



Fig. 9 : CHC development, 3rd injection phase, anaerobic (left) and aerobic (right) influenced destination

ACCOMPANYING MODELING WITH DIFFERENT **3D MODELING COMPONENTS**





Fig. 11: Visualization of calculated initial heterogeneous gas distribution after 100 min injection

- Geological 3D structural model (GMS)
- Hydrogeological 3D flow model (MODFLOW)
- Reactive transport model GMS-RT3D
- Reactive 2-phase transport model (TOUGH II)



Fig. 12: Simulated PCH degradation, 30 and 50 days after hvdroaen iniection

RESULTS AND CONCLUSIONS

The application of the new gas injection technology was designed, built and tested on a site down gradient of a large CHC contaminated aquifer in Leipzig, Germany. In general, the functionality of the efficient and low cost gas injection approach was proven; however, the process of CHC degradation was strongly influenced by other competing reaction processes due to the complex local site conditions. Therefore the quantification of a single processes was difficult to show and further development work is necessary. In addition, the results showed that the complete remediation scenarios can be accurately simulated by modeling.

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